WHAT IS CLAIMED IS:

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- 1. A carrier for the catalyst to be used in the production of ethylene oxide, obtained by adding an aluminum compound, a silicon compound, and an alkali metal compound to a low-alkali content α -alumina powder having an alkali metal content in the range of 1 70 m.mols/kg of powder and calcining the resultant mixture, the aluminum compound content as reduced to aluminum being in the range of 0 3 mols/kg of carrier, the silicon compound content as reduced to silicon in the range of 0.01 2 mols/kg of carrier, and the alkali metal content as reduced to alkali metal in the range of 0.01 2 mols/kg of carrier respectively in said carrier.
- 2. A carrier according to claim 1, wherein the atomic ratio of said alkali metal content in said powder/said alkali metal content in said carrier is in the range of 0.0001 0.8.
- 3. A carrier according to claim 1, wherein said alkali 20 metal content in said α -alumina is in the range of 3 30 m.mol/kg of powder.
 - 4. A carrier according to claim 1, wherein the secondary particle average diameter of said α -alumina is in the range of 50 100 μ m of powder.
- 5. A carrier according to claim 1, wherein the BET specific surface area of said α -alumina is in the range of $1-4~\text{m}^2/\text{g}$.
 - 6. A carrier according to claim 1, wherein said aluminum compound content as reduced to aluminum is in the range of 0.01 2 mols/kg of carrier and said alkali metal compound content in the range of 0.02 0.5 mol/kg of carrier in said carrier.

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- 7. A method for the production of a carrier to be used in the production of ethylene oxide, which comprises mixing a low-alkali content α -alumina powder having an alkali metal content in the range of 1 70 m.mols/kg of powder with an aluminum compound, a silicon compound, and an alkali metal compound at ratios such that in the produced carrier, the aluminum compound content as reduced to aluminum is in the range of 0 3 mols/kg of carrier, the silicon compound content as reduced to silicon in the range of 0.01 2 mols/kg of carrier, and the alkali metal compound content as reduced to alkali metal in the range of 0.01 2 mols/kg of carrier, forming the resultant mixture in a prescribed shape, and then calcining the formed mixture.
- 8. A method according to claim 7, wherein the atomic ratio of said alkali metal content in said powder/said alkali metal content in said carrier is in the range of 0.0001 0.8.
 - 9. A method according to claim 7, wherein said alkali metal content in said α -alumina is in the range of 3 30 m.mols/kg of powder.
 - 10. A method according to claim 7, wherein said alumina has an average particle diameter in the range of 50 100 μm
- 11. A method according to claim 7, wherein said α 25 alumina has a BET specific surface area in the range of 1
 4 m²/g.
 - 12. A method according to claim 7, wherein said aluminum compound content as reduced to aluminum is in the range of 0.01 2 mols/kg of carrier and said alkali metal compound content in the range of 0.02 0.5 mol/g of carrier respectively in said carrier.

Support

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- 13. A catalyst for use in the production of ethylene oxide, obtained by depositing a silver-containing catalytic component on a carrier set forth in claim 1.
- 14. A catalyst according to claim 13, wherein the amount of silver deposited is in the range of 1 30 wt. % based on the weight of said catalyst.
- 15. A catalyst according to claim 14, wherein an alkali metal is deposited as a reaction promoting agent in an amount in the range of 0.001 2 wt. %, based on the weight of the catalyst.
- 16. A catalyst according to claim 15, wherein said alkali metal is cesium or rubidium.
- 17. A method for the production of a catalyst to be used for the production of ethylene oxide, characterized by depositing a silver-containing catalytic component on a carrier set forth in claim 1 and then calcining the resultant composite.
- 18. A method according to claim 17, wherein said calcination is effected in the current of an inert gas at a temperature in the range of 400 700°C.
- 19. A method for the production of ethylene oxide, characterized by subjecting ethylene to catalytic gas phase oxidation with a molecular oxygen-containing gas in the presence of a catalyst set forth in claim 13.

- Add BD)